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# Chemo-enzymatic conversions of biomass constituents

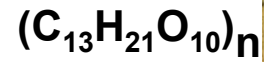
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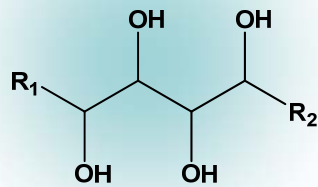
# Nature's Chemical Diversity for the Diversity of Chemical Products



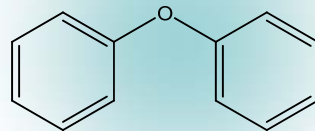
**Biomass**



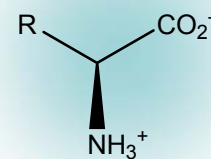
Carbohydrates



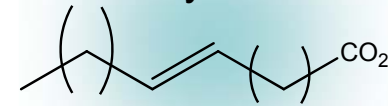
Lignin



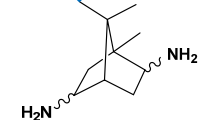
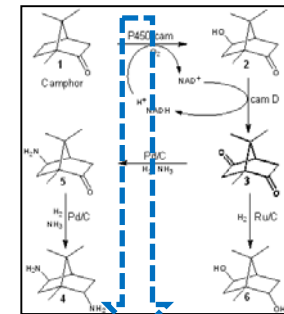
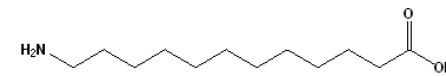
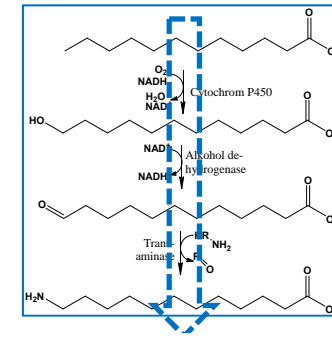
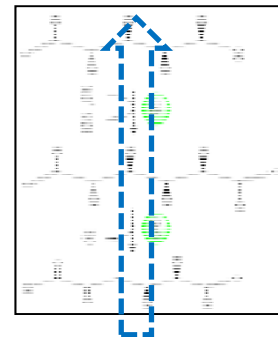
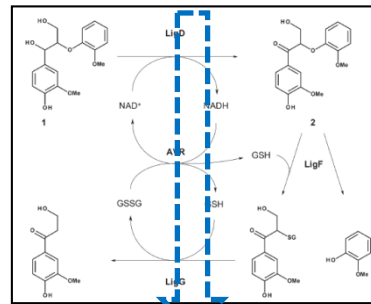
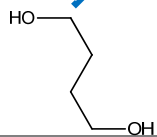
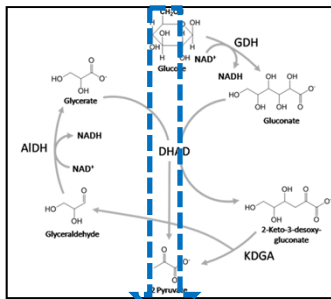
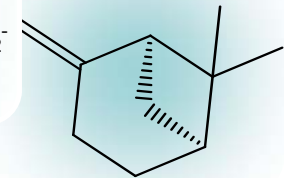
Amino acids



Fatty acids



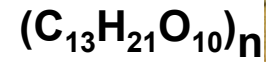
Terpene



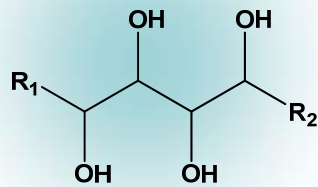
## Nature's Chemical Diversity for the Diversity of Chemical Products



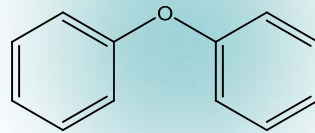
**Biomass**



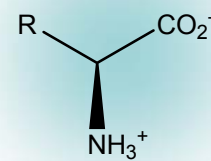
Carbohydrates



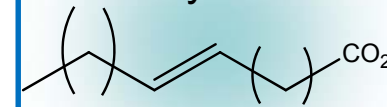
Lignin



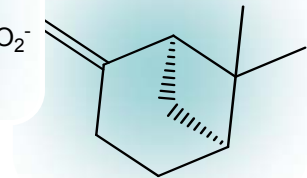
Amino acids



Fatty acids



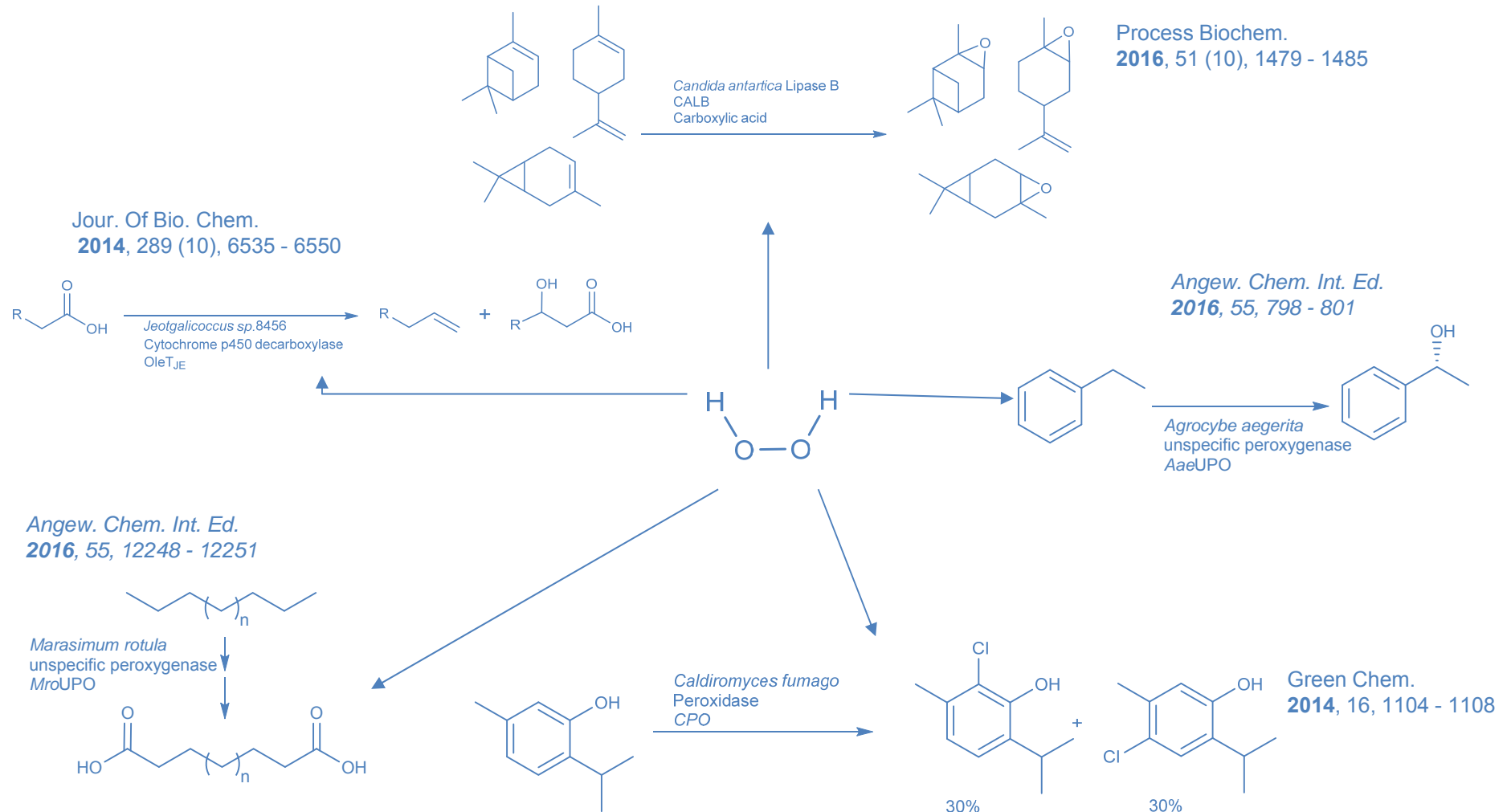
Terpene



**Over-  
functionalized**

**Under-  
functionalized  
=> Oxidation**

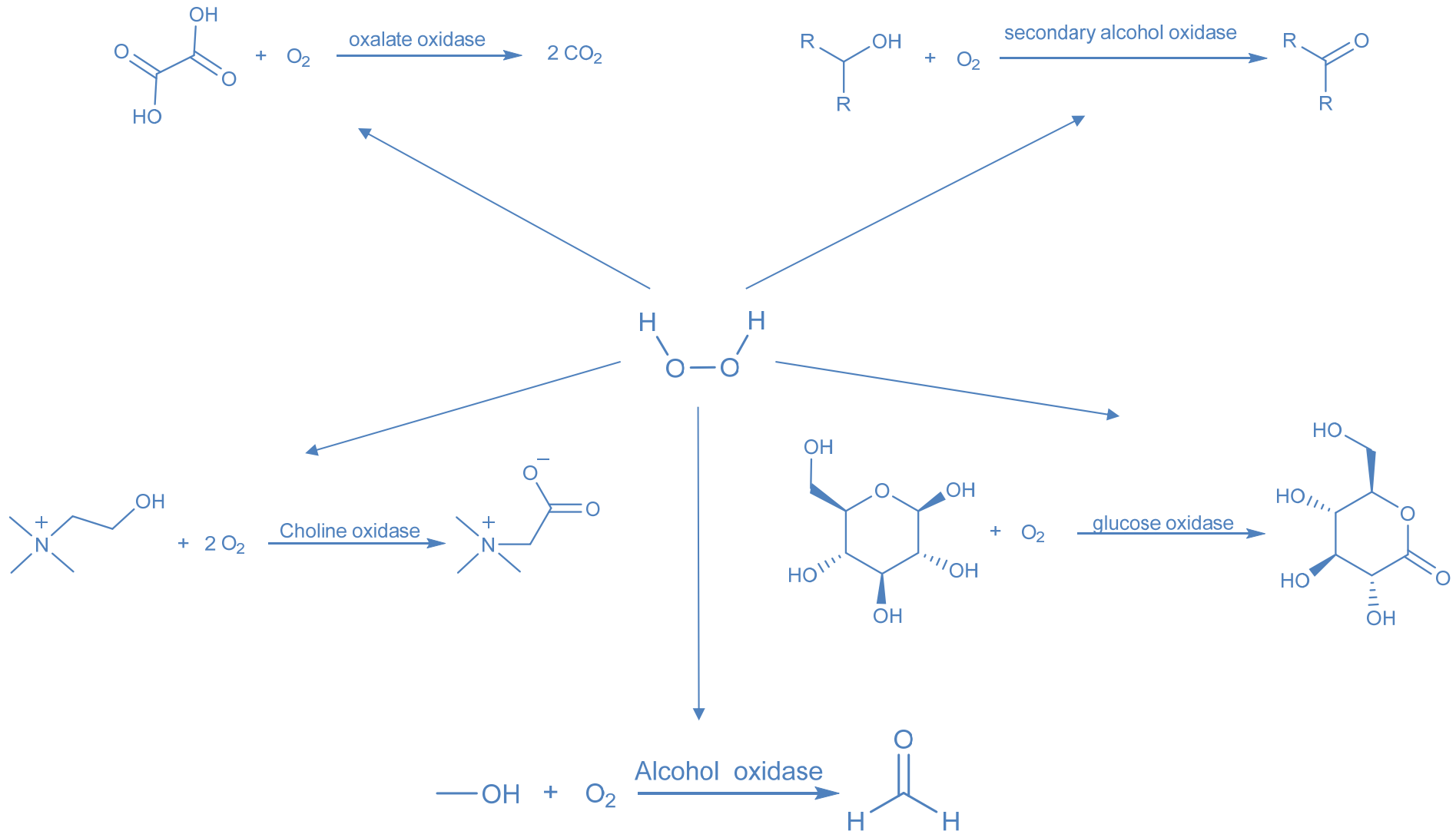
# Enzymatic reactions dependent on H<sub>2</sub>O<sub>2</sub>



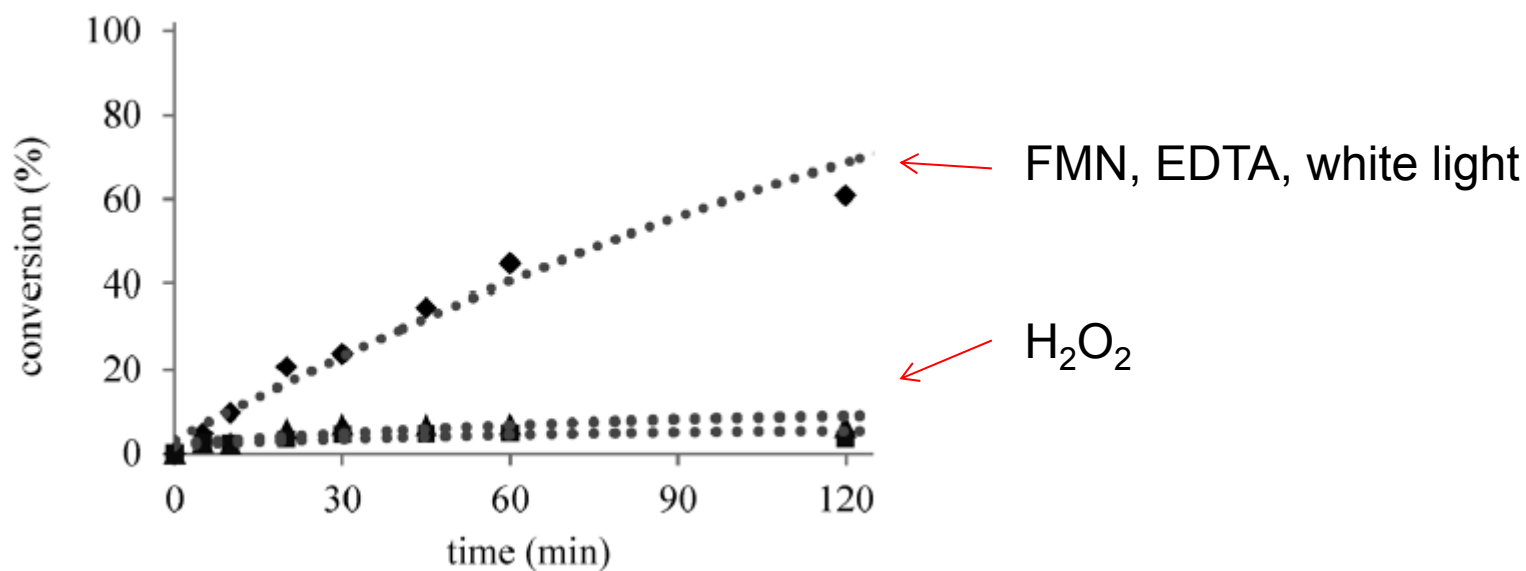
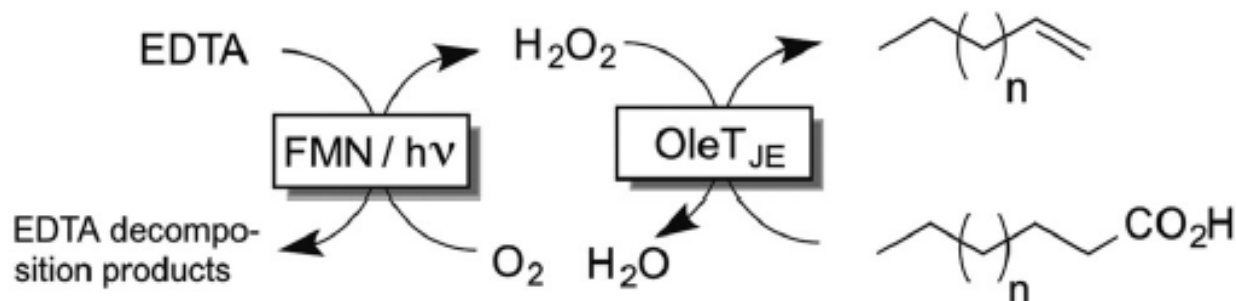
# H<sub>2</sub>O<sub>2</sub> synthesis methods

- Chemical
  - Anthraquinone autooxidation process
  - Shell 2-propanol process
  - Direct synthesis: H<sub>2</sub> and O<sub>2</sub>
- Electrochemical
  - Degussa-Wissenstein Process
  - Münchner Process
- Photocatalytic
  - Carbon nitride catalysts
  - Flavin dependent generation
- Enzymatic
  - Oxidase (E.C 1.1.3.X)

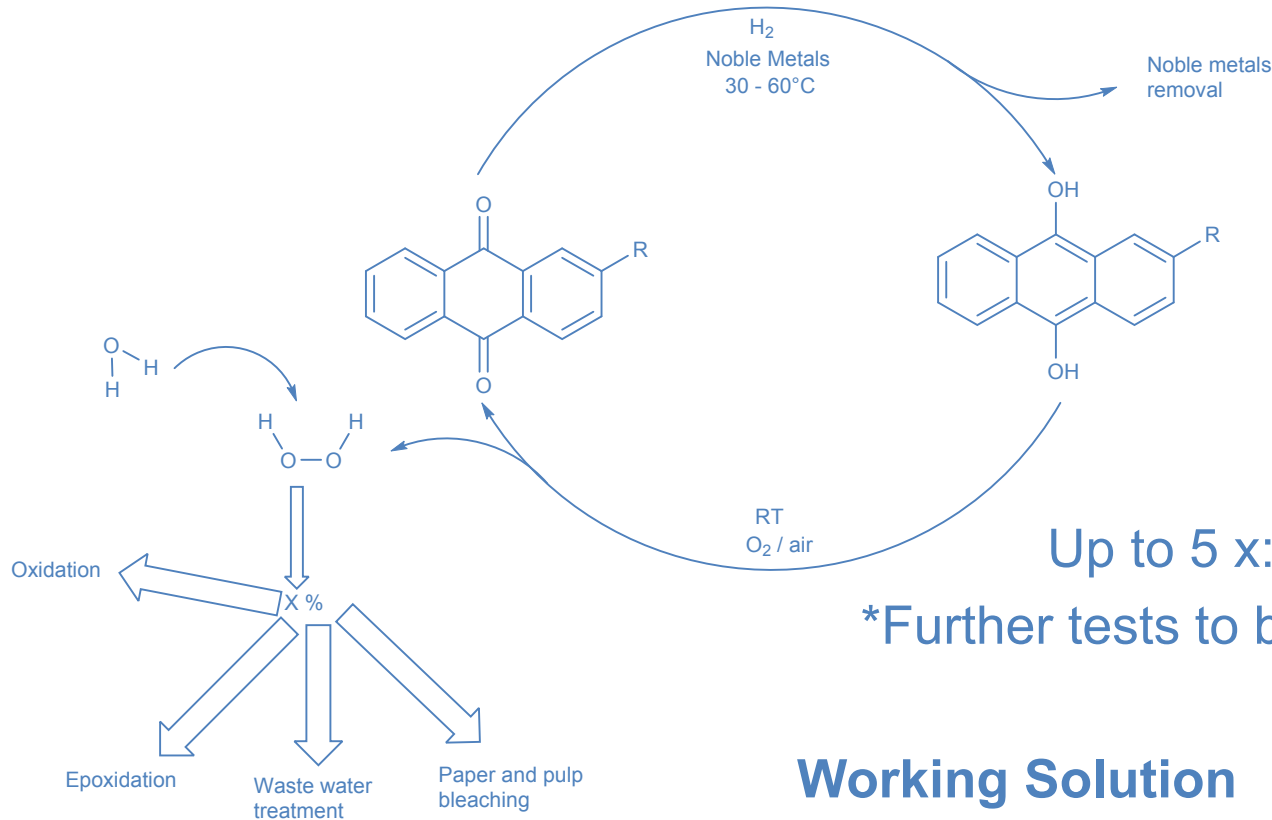
# Enzymatic H<sub>2</sub>O<sub>2</sub> formation



# Oxidative Decarboxylation for long-chain Olefins



# Anthraquinone /Autooxidation Process



Pressure: 1 – 1.1 bar  
Temperature: 45 - 60°C  
 $\text{H}_2\text{O}_2$ : 92 – 100 %

Up to 5 x: no catalyst inactivation\*

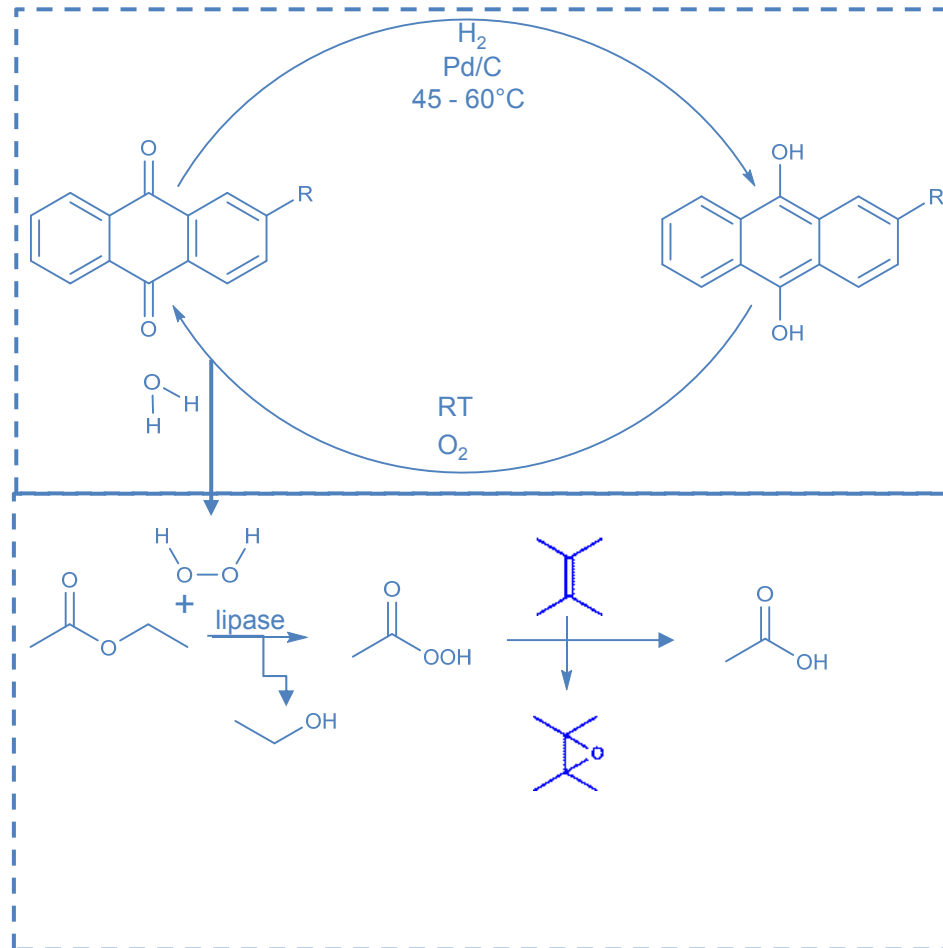
\*Further tests to be done with recyclability

## Working Solution

60% mesitylene & 40% tributyl phosphate

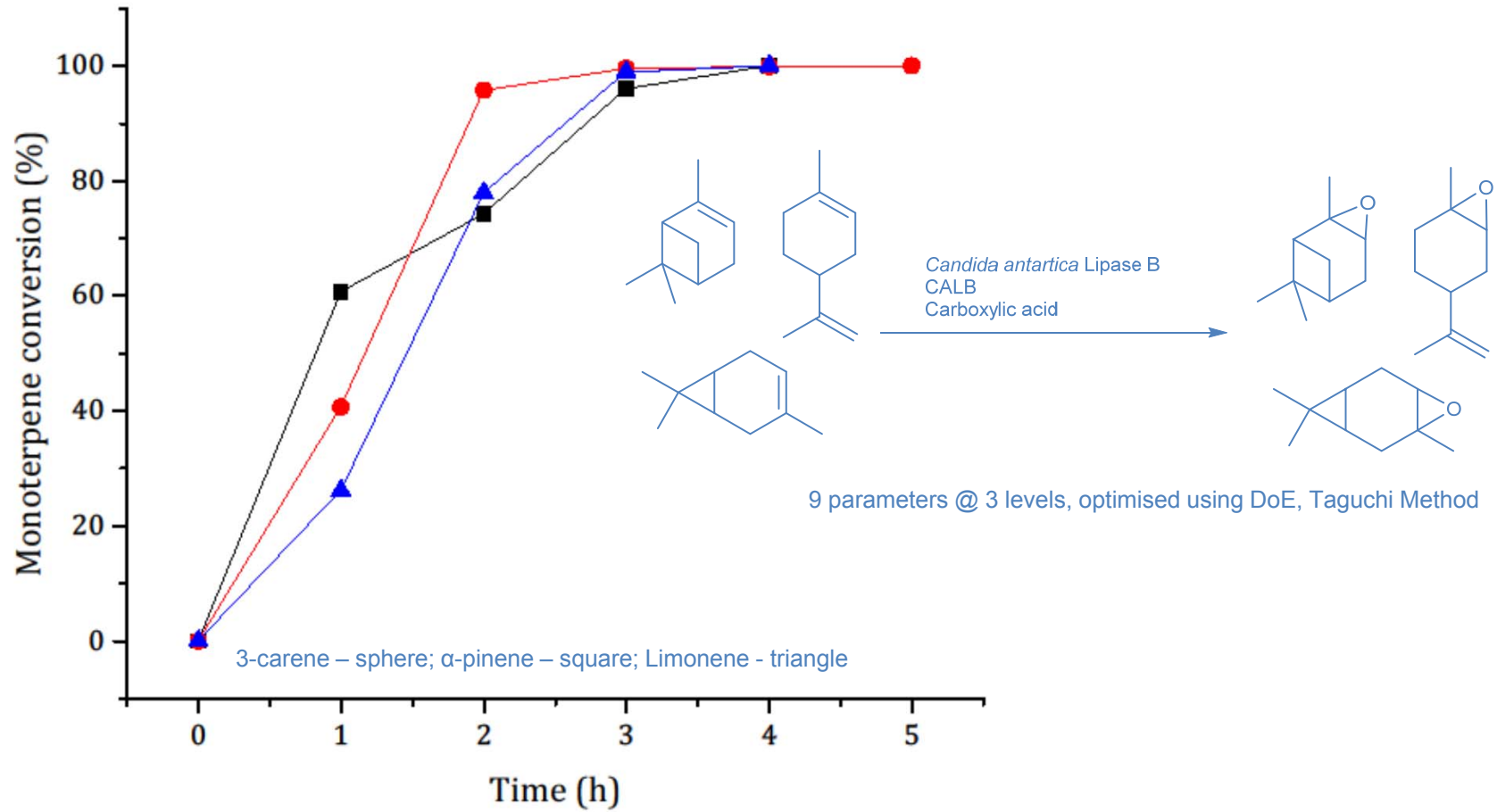


## Combined Approach – 1.0



- Semi-batch process
- 60% toluene + 40% ethyl acetate
- Ethyl acetate hydrolysis to peroxyacetic acid and ethanol
- 75 – 85% epoxide yield
- Disadvantage
  - Only single run possible
  - Fresh solvent for every run
- Modified approach developed

# Epoxidation of 3-carene, limonene and $\alpha$ -pinene



## Biosurfactants

**Petroleum**



**Process**

**Petro-based surfactants**

Synthesis: often high carbon footprint; products show limited biodegradation

### **Renewable resources**

- Plant biomass
  - Terpenes
  - Sugars, fatty acids
- Animal biomass
  - Amino sugars

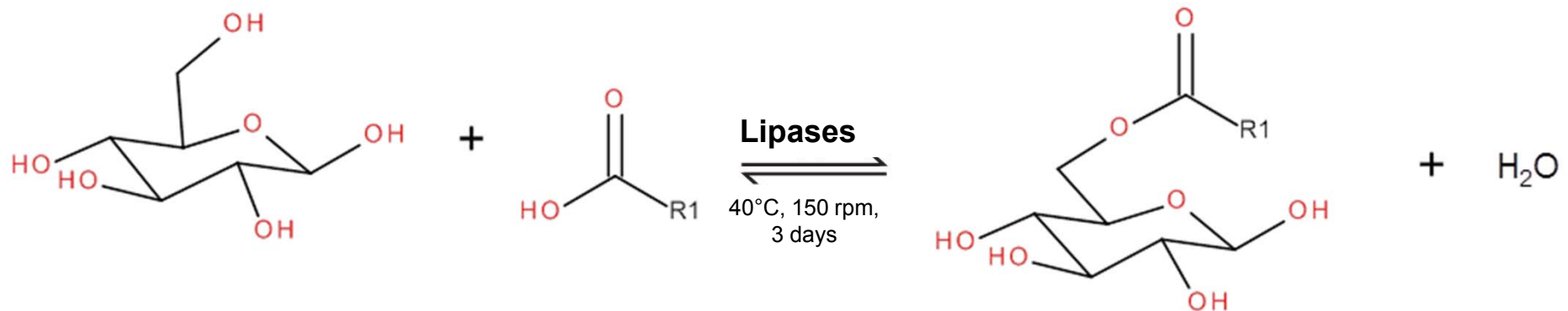


**Biocatalysis**

### **Biosurfactants**

- Bio-based,  
biodegradable

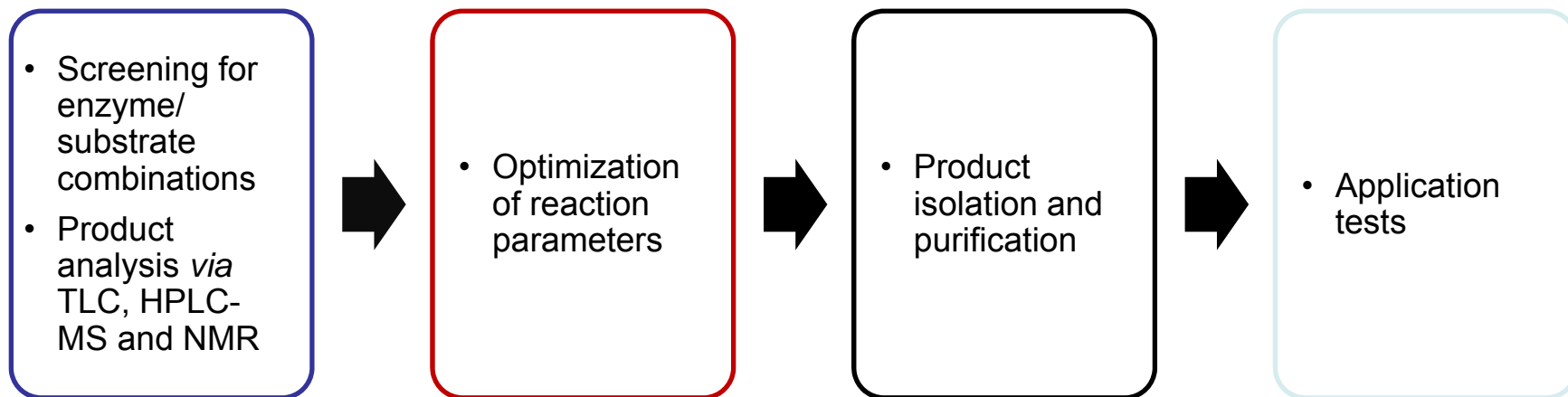
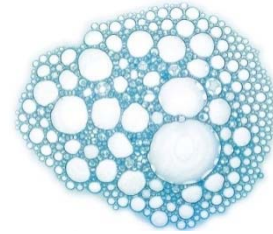
## Biosurfactants – Amphiphilic Sugar Esters



- **lipases (EC 3.1.1.3)** catalyze the formation esters in organic solvent
- esterification of primary and secondary alcohols possible
- water has to be removed during course of reaction to prevent ester hydrolysis
- challenge: system contains hydrophilic, hydrophobic and amphiphilic components

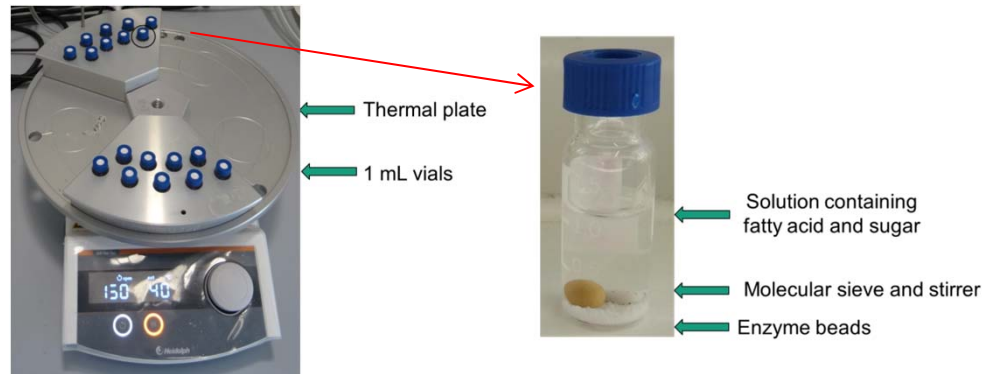
## Lubricants and Bio-based Surfactants from Renewable Resources

- Synthesis of new biosurfactants from vegetable oils, fatty acids, terpenes and sugars
- Characterization of novel surfactants via TLC, HPLC-MS, NMR and application tests

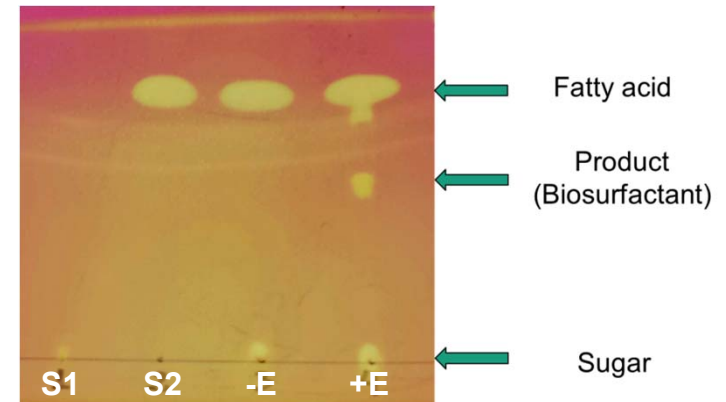


## Enzymatic Synthesis of Surfactants - Procedure

- Screening of enzymes and substrates:



### TLC



Up-scaling to multi-gram scale:

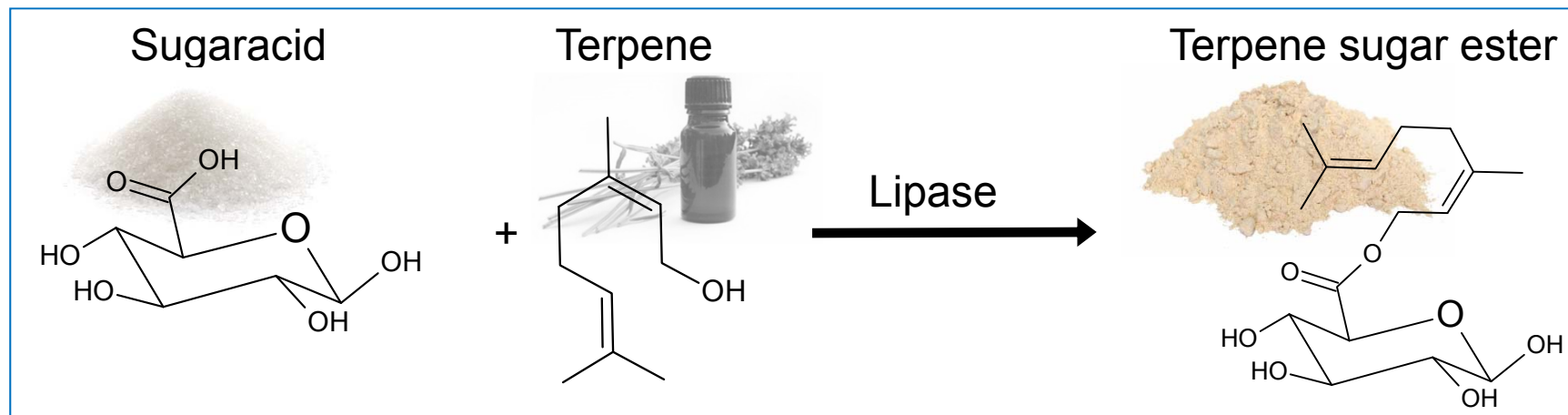


exclusive access to:

- bio-based building blocks
- enzymes
- process routes

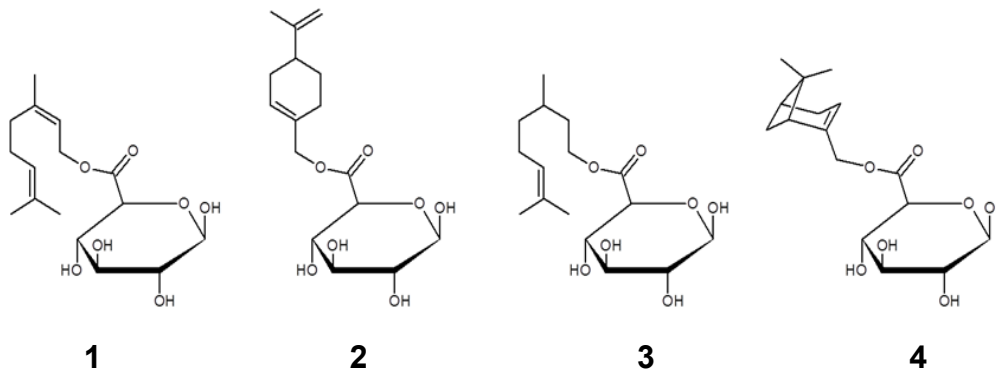
## Lubricants and Bio-based Surfactants from Renewable Resources

- Synthesis of new bio-surfactants from **terpenes** and sugars
  - terpenes: underexploited waste stream
  - suitable for lipase mediated epoxidation and follow up chemistry
  - bioactivity



## Lubricants and Bio-based Surfactants from Renewable Resources

- terpene sugar esters



Conversion of terpenols with glucuronic acid:  
CalB (Novozymes 435)  
40 mM equimolar substrate in *t*-butanol, 60 °C for 48 h

Terpenoid alcohol	Alcohol type	Product formation
Nerol (1)	P	+++
Geraniol	P	+++
Myrtenol (4)	P	++
Perillyl alcohol (2)	P	+++
Citronellol (3)	P	+++
Carveol	S	-
Verbenol	S	-
Linalool	S	-
Isoborneol	S	-
Terpineol	T	-

Product formation monitored by TLC

P: Primary alcohol;

S: secondary alcohol;

T: tertiary alcohol.

*J. G. Ortiz-Tena et al., in prep.*

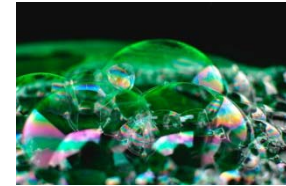
[www.biosurf.fraunhofer.de](http://www.biosurf.fraunhofer.de)

Project acronym: BioSurf.  
Project no: EIB.10.039

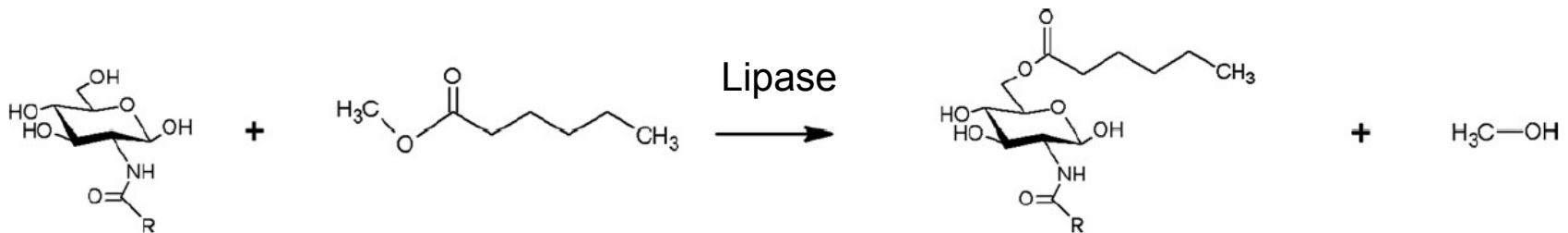


## Lubricants and Bio-based Surfactants from Renewable Resources

- Synthesis of new bio-surfactants from **chitin** derived precursors

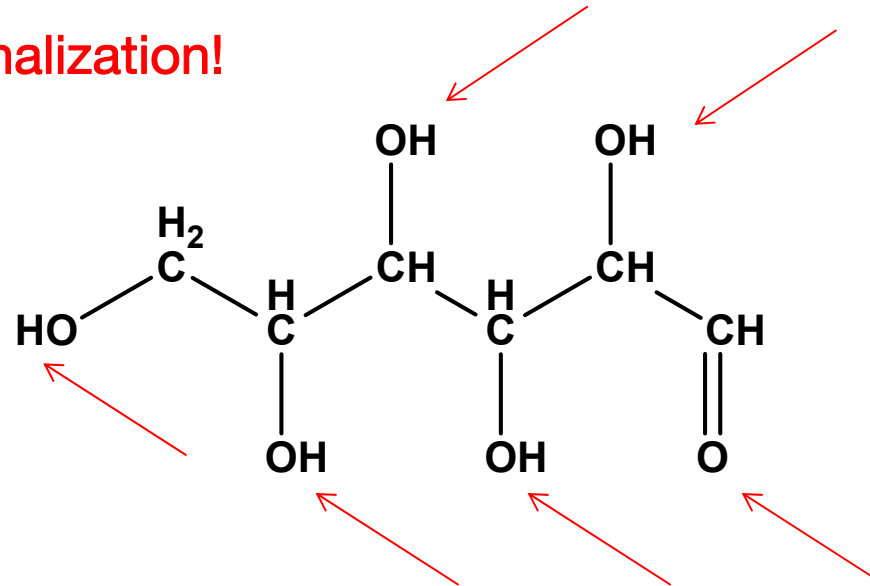


Chitin monomers

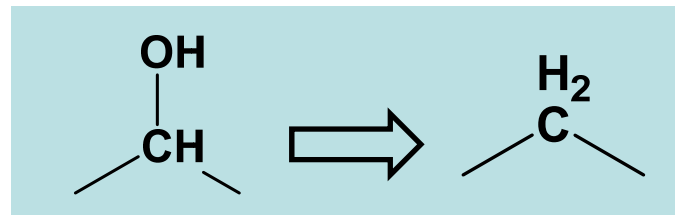


# Carbohydrates as substrates for chemistry

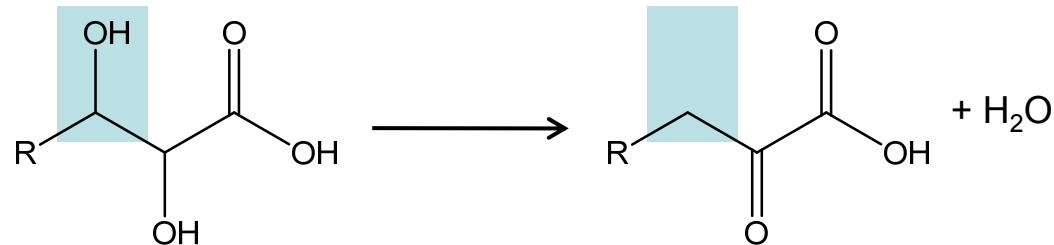
**Problem of over-functionalization!**



**The task is defunctionalization!**

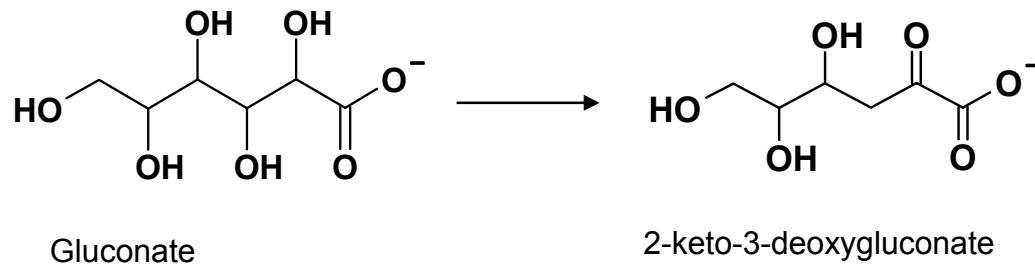


## One way for dehydration: Dihydroxy Acid Dehydratase



- $\alpha$ - $\beta$ -dehydratase (EC 4.2.1.x)
- dehydration of 2,3-dihydroxy-isovaleric acid to  $\alpha$ -ketoisovaleric acid
- Iron-Sulfur Cluster Enzymes

***DHAD from *Sulfolobus solfataricus**** (pH 2-3, T of 75-80 °C)

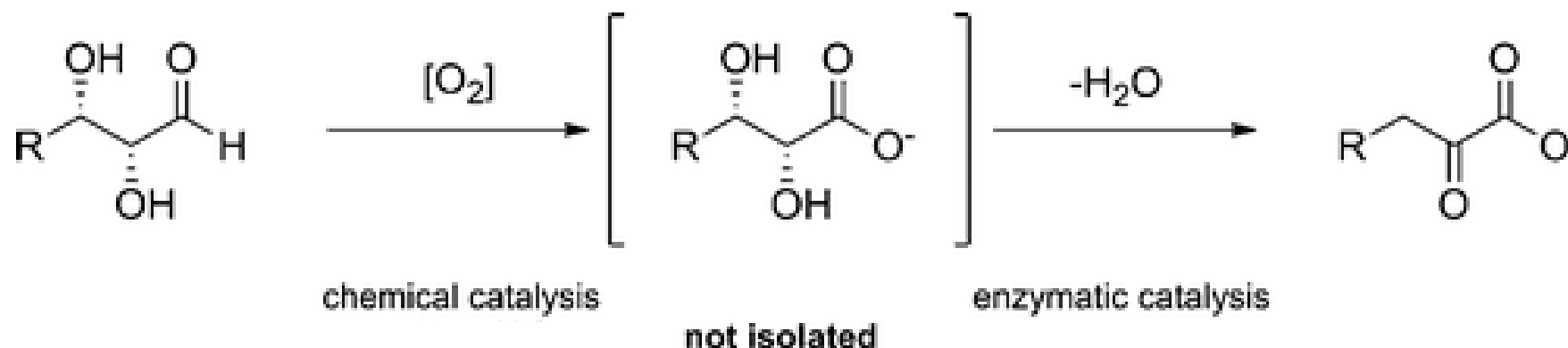


pH<sub>opt</sub> of 6.2  
 T<sub>opt</sub> = 80 °C  
 Activity ca. 5 u/mg  
 TTN: ca. 35000

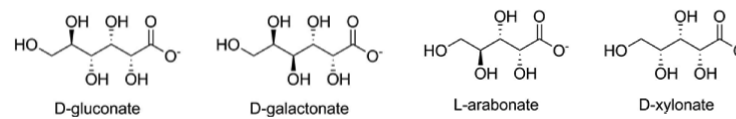
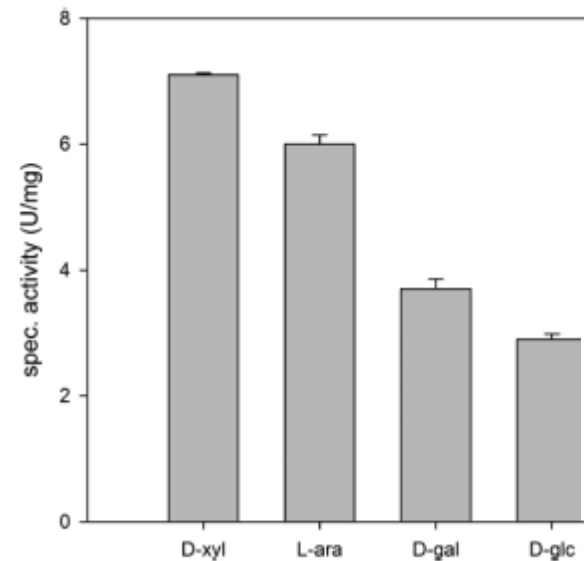
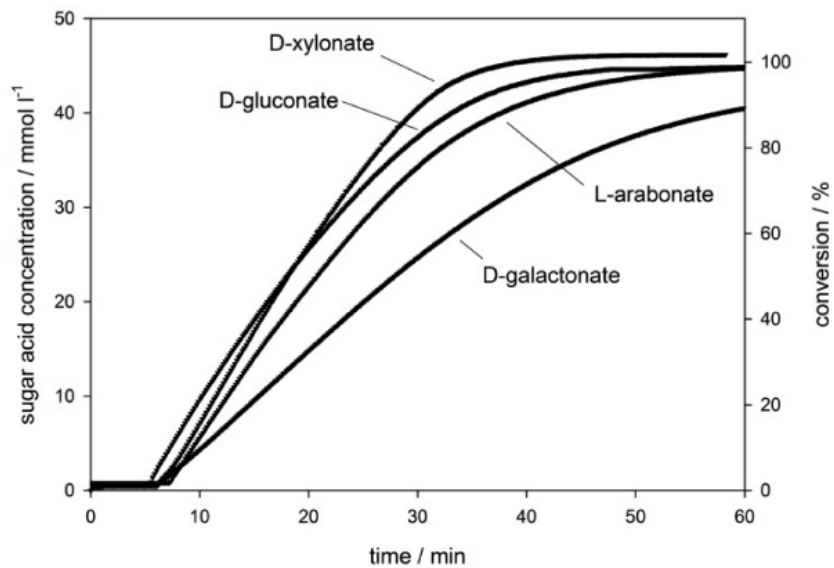
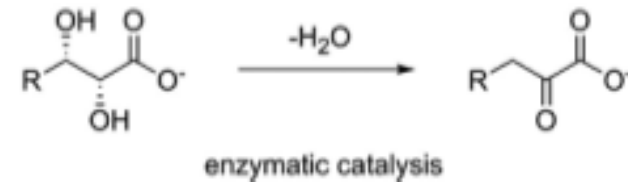
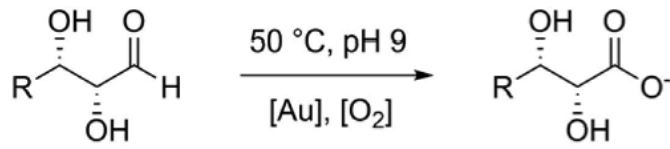
## Production of $\beta$ -desoxy- $\alpha$ -keto acids from carbohydrates

- => Represent a first partially defunctionalized intermediate towards biobased building blocks such as adipic acid, muconic acid, succinic acid, or 1,4 butanediol
- => Building block for organic synthesis because a vicinal electrophilic and nucleophilic carbon pair is obtained from chemically indifferent hydroxymethylene groups
- => Especially for carbohydrates: a generic aldol building block is formed

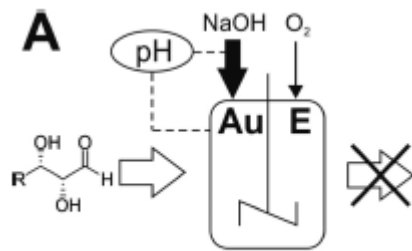
### Combination of Heterogeneous Catalysis and Enzyme Catalysis



# Production of $\beta$ -desoxy- $\alpha$ -keto acids from carbohydrates

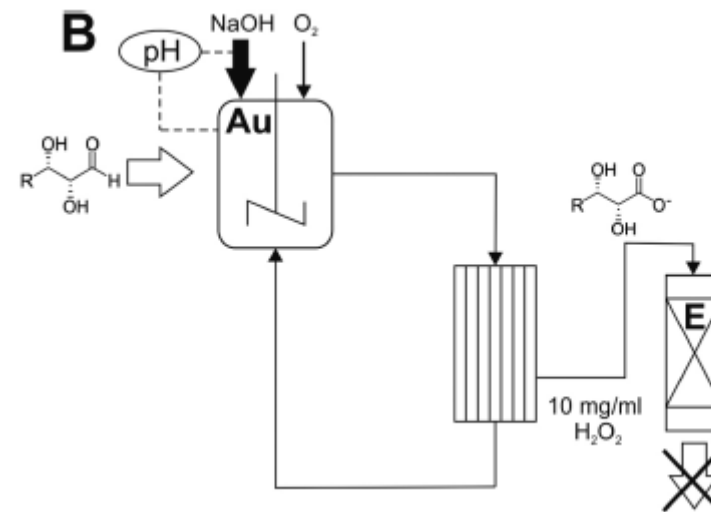


# Reaction Design for the Compartmented Combination of Heterogeneous and Enzyme Catalysis



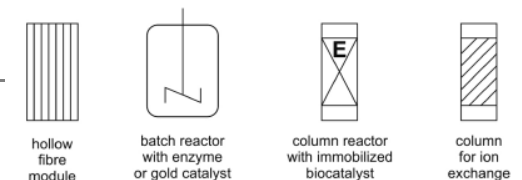
## One pot

- Compromise for conditions
- Mutual inactivation
- Mechanical barriers (alginate capsules, „Tea bag“ etc.) reduced inactivation but also activity

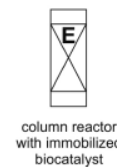
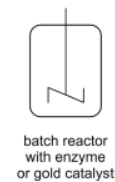
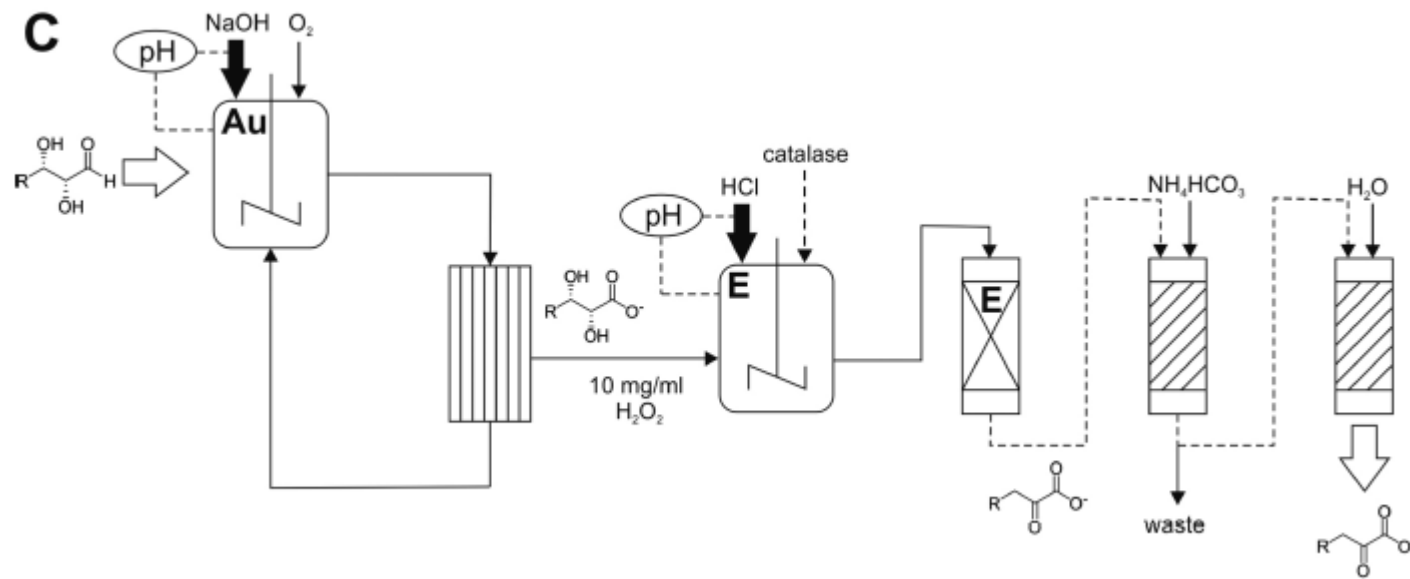


## Separation

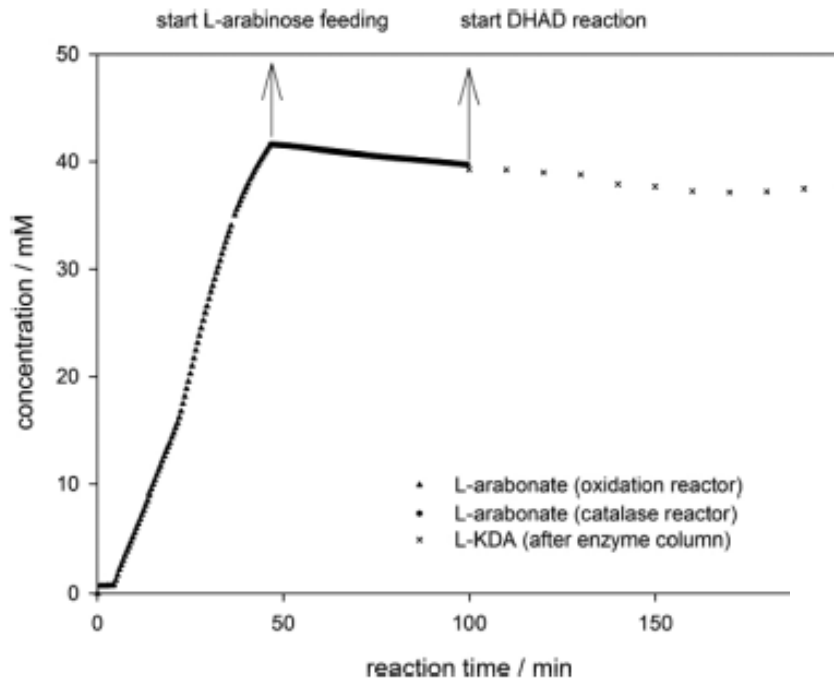
- Continuous-flow reactor system
- Cross-flow filtration for catalyst separation



# Reaction Design for the Compartmented Combination of Heterogeneous and Enzyme Catalysis



## Reaction Design for the Compartmented Combination of Heterogeneous and Enzyme Catalysis



**Table 1. Continuous Flow Transformation of Different Sugars to KDS**

substrate	flow rate (ml min <sup>-1</sup> )	av concn (mM)	yield b.p. (%) <sup>a</sup>	yield a.p. (%) <sup>a</sup>
L-arabinose	1.0	38	84	58
D-xylose	1.0	31	69	n.d. <sup>a</sup>
D-galactose	0.5	39	87	n.d. <sup>a</sup>
D-glucose	0.3	41	91	86

<sup>a</sup>D-KDX and D-KDGal showed degradation during the ion exchange purification step. b.p. before purification, a.p. after purification.

- ⇒ First step towards adipic acid, muconic acid and others
- ⇒ Increase of substrate concentration with optimized enzyme



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## Summary

### In-situ peroxide production

- Semi-continuous system for high concentration of  $H_2O_2$
- Application for Epoxide production

### Bio-surfactant

- Toolbox for biocatalytic synthesis of ionic and non-ionic surfactants from biomass
- New building blocks from terpenes as hydrophobic moiety
- Development of efficient DSP strategies of the amphiphilic products

### Carbohydrate based building block

- First step towards adipic acid, muconic acid and others
- Enzyme variants with higher activity and stability are at hand